Results from Four Full-Scale Field Tests of ACI for Control of Mercury Emissions

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Outline

- Background on DOE NETL Program
- Background on Sorption of Hg on Solid Sorbents
 - Implications on variability of ICR results
- Details of Salem Harbor Program
- Summary of other three field tests
- Conclusions on ACI



ADA-ES Hg Control Program

- Full-scale field testing of sorbent-based mercury control on non-scrubbed coal-fired boilers
- Primary funding from DOE National Energy Technology Laboratory (NETL)
- Cofunding provided by:
 - Southern Company
 - We Energies
 - PG&E NEG
 - EPRI
 - Ontario Power Generation
 - TVA
 - First Energy
 - Kennecott Energy
 - Arch Coal
 - Hamon
 - NORIT



DOE/NETL Test Sites

Test Site	Coal	Particulate Control	Test <u>Dates</u>
Alabama Power Gaston	Bituminous	HS ESP COHPAC FF	Spring 2001
Wisconsin Electric Pleasant Prairie	PRB	Cold Side ESP	Fall 2001
PG&E NEG Brayton Point	Bituminous	Cold Side ESP	Summer 2002
PG&E NEG Salem Harbor	Bituminous	Cold Side ESP	Fall 2002



Differences in Coal and Flue Gas Characteristics for the Four DOE Sites

Plant	Coal	Hg (ppm)	Chlorine (ppm)
We Energies Pleasant Prairie	PRB	0.11	8
Alabama Power Gaston	Washed Eastern Bit	0.14	169
PG&E NEG Brayton Point	Eastern Bit	0.03	2000-4000
PG&E NEG Salem Harbor	South Amer. Bituminous	0.03-0.08	206



Activated Carbon Storage and Feed System





Powdered Activated Carbon Injection System



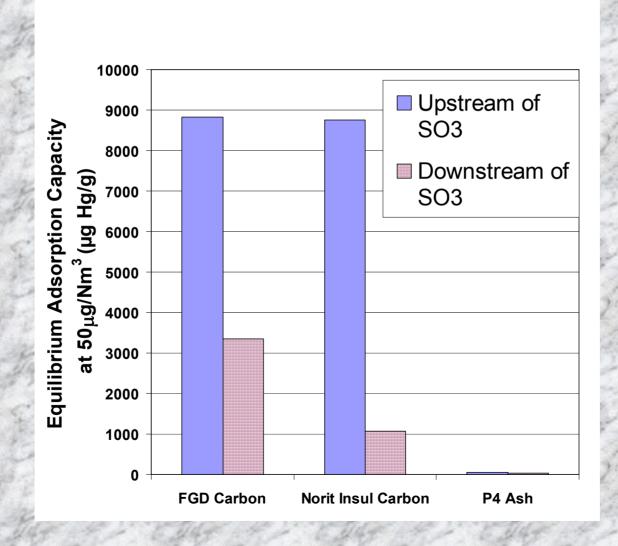


Capture of Vapor Phase Hg by Solid Sorbents

- Mass Transfer Limits (getting the Hg to the sorbent):
 - Removal increases with particle concentration
 - » Optimize by increasing mass loading and decreasing particle size
 - Produces percentage removal independent of concentration; and
 - Particle control device (FF vs ESP) is a critical parameter.
- Sorbent Capacity (ability to retain Hg) depends upon:
 - Sorbent characteristics such as surface area, capacity, and reactivity
 - Temperature: decreases at higher temperatures
 - Mercury concentration; and
 - Concentrations of SO₃ and other contaminants.

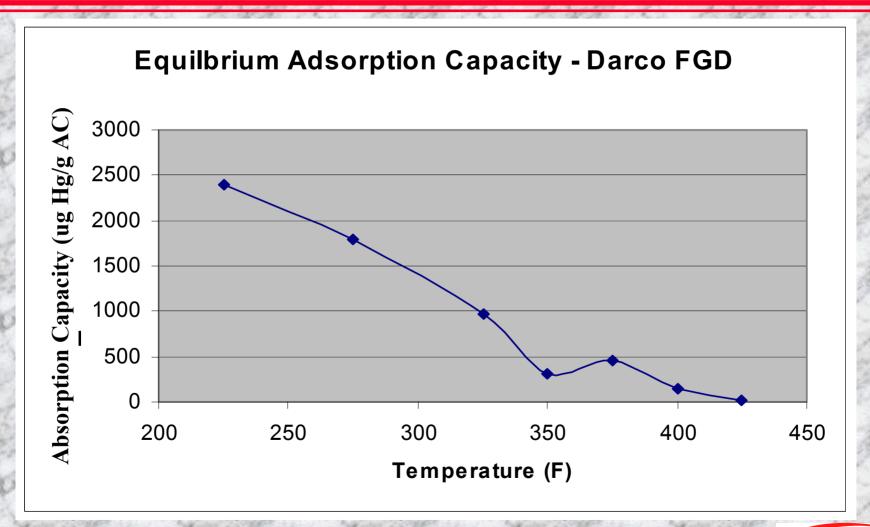


Equilibrium Adsorption Capacities at 250°F Upstream and Downstream of SO₃ Injection



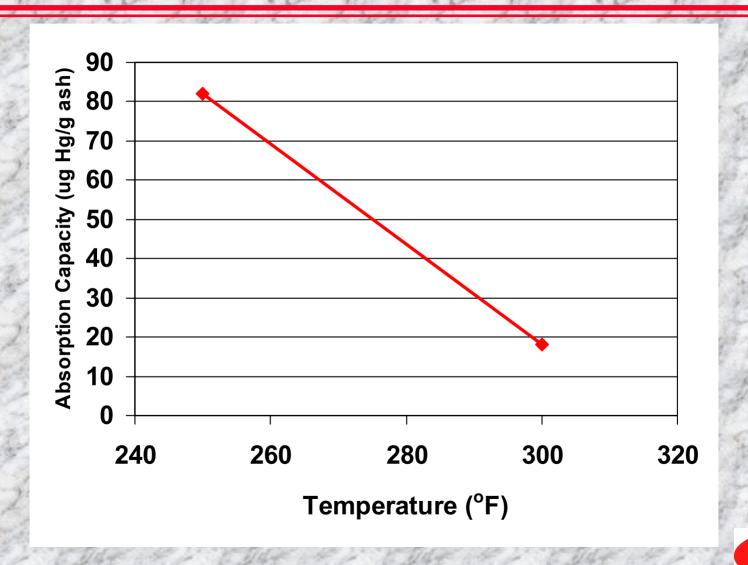


Adsorption Capacity vs. Temperature





Adsorption Capacity of LOI Carbon





Equivalent Mass of Carbon Basis

LOI %	Flue Gas Concentration (Ib/MMacf)
15	36
20	48
25	60
30	72
35	84



PG&E NEG Salem Harbor Unit 1

- 85 MW B&W Radiant Boiler
- NOx Control: SNCR
- PM Control: ESP with an SCA of 474 ft²/kacfm
- Coal: South American Bituminous
 - Sulfur (%): 0.63
 - Mercury: 0.03 0.08 ug/g
 - Chlorine: 206 ppm
- LOI (Loss on Ignition, Carbon Content): 25-35%



Baseline Results

Location	Particle Bound	Oxidized, Hg ²⁺	Elemental, Hg ⁰	Total, Hg
Inlet – Location #1 (μg/dscf)*	9.27	0.08	<0.23	9.58
Outlet – Location #3 (μg/dscf)*	<0.23	0.27	<0.38	<0.88
RE (%)	97.14	-211.65	-75.27	90.81



Objectives of Hg Test Program at Salem Harbor

- Understand the reasons that high Hg removal levels occurred under baseline (no ACI) conditions
- Document the impact of the SNCR system on Hg control
- Document the impact of LOI on Hg control
- Document impact of temperature on Hg control
- Evaluate impact of ACI

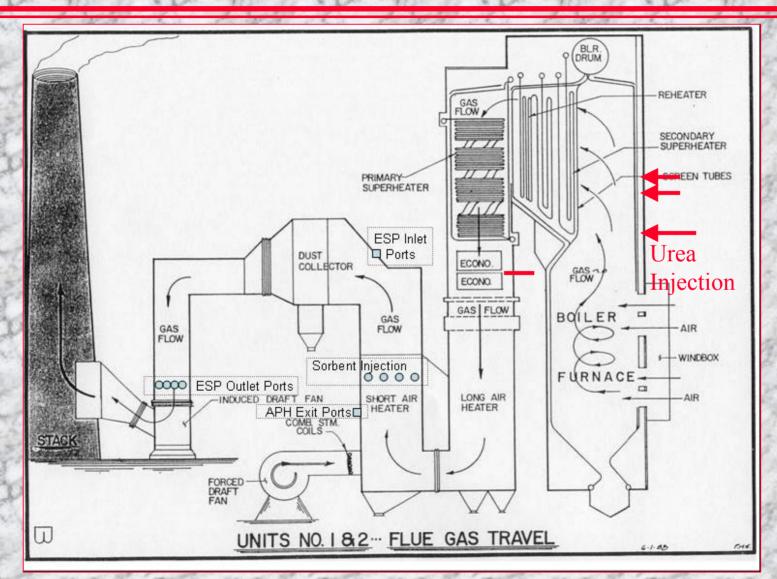


Operating Parameters

- SNCR operation:
 - On/off tests by turning off injection of urea
- LOI:
 - Decrease LOI by operating at high excess air at low load
- ESP Temperature:
 - Increase temperature by using steam coils to increase temperature of air entering air preheater

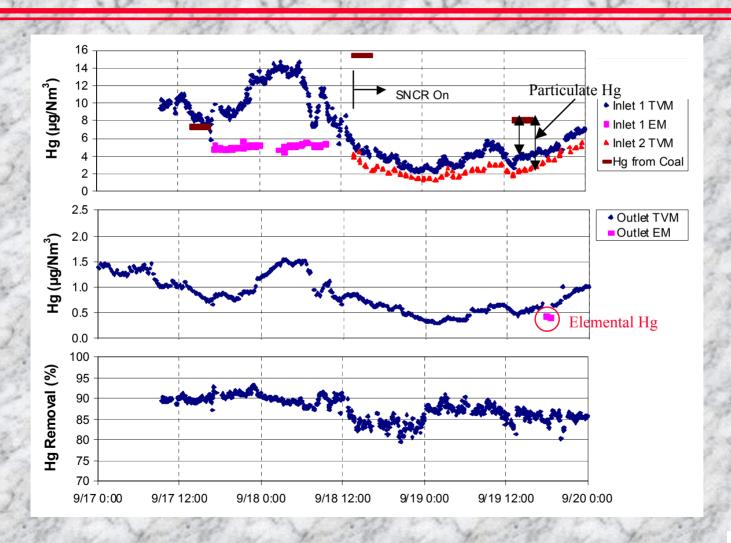


Flue Gas Path



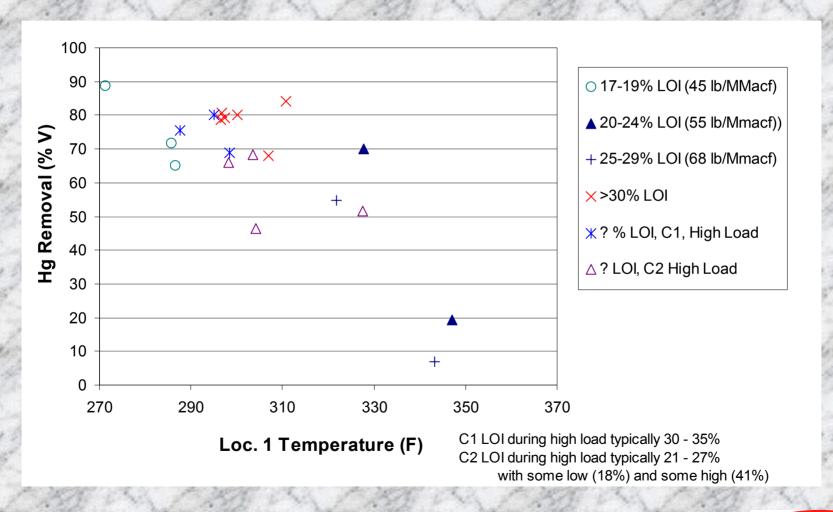


SNCR On/Off



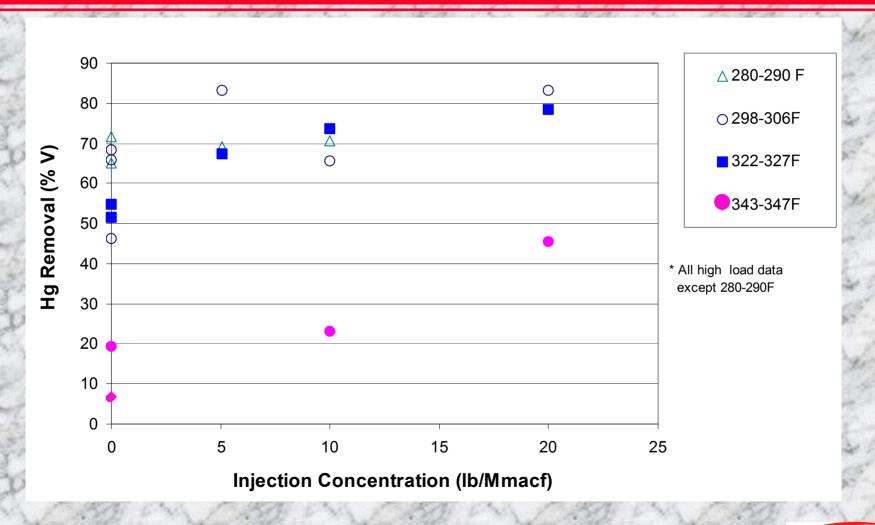


Hg RE% vs. Temperature (No ACI)





Hg RE% vs. Injection Concentration





Conclusions of Hg Control Testing at Salem Harbor

- No impact of SNCR operation on Hg removal
- At standard operating temperatures (300°F), reducing LOI from 30-35% to 15-20% has minimal impact on Hg removal
- At Salem Harbor, temperature has greater impact on mercury removal than LOI
- LOI has minimal capacity and is impacted by temperature and the presence of acid gases
- Activated carbon has excess capacity at moderate temperatures and less sensitive to changes in coal and flue gas conditions
- Activated carbon was less effective capturing mercury at higher temperatures (> 340°F)



Summary of Results from Other Three Field Tests



Removal of Mercury Species with PAC on Bituminous and Subbituminous Coal

Bituminous with FF

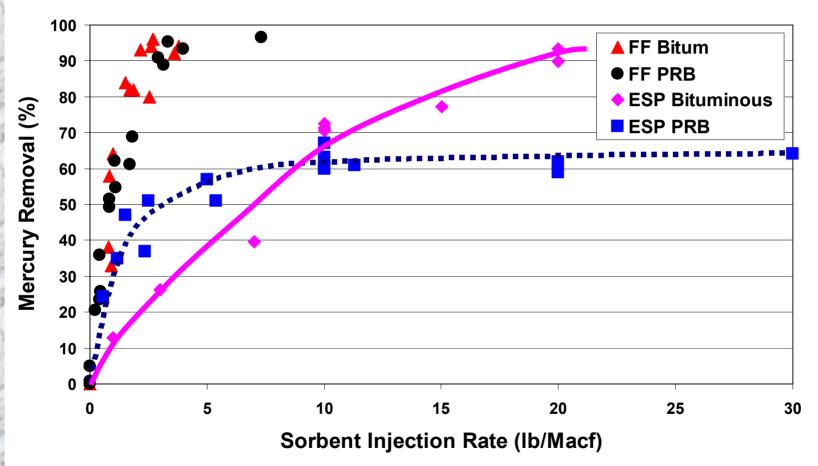
	PARTICULATE	OXIDIZED	ELEMENTAL	TOTAL
PAC Injection	μg/m³	μg/m³	μg/m³	μg/m³
COHPAC Inlet	0.23	6.37	4.59	11.19
COHPAC Outlet	0.12	0.91	0.03	1.05
Removal Efficiency	45.6%	85.7%	99.3%	90.6%

Subbituminous with ESP

	PARTICULATE	OXIDIZED	ELEMENTAL	TOTAL
PAC Injection	μg/m³	μg/m³	μg/m³	μg/m³
ESP Inlet	0.98	1.73	14.73	17.44
ESP Outlet	0.00	0.44	4.27	4.71
Removal Efficiency	y 100.0%	74.5%	71.0%	73.0 %



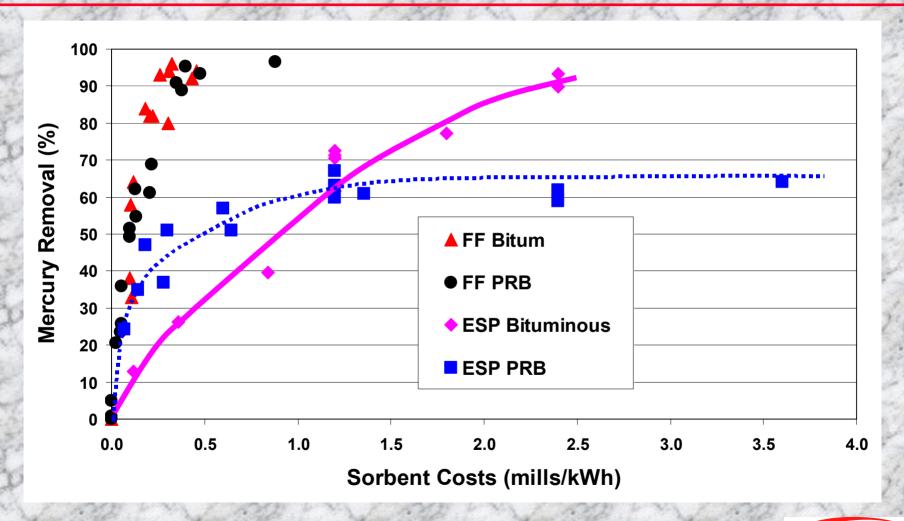
Mercury Removal with PAC Upstream of FFS and ESPs







Comparison of Sorbent Costs for a Fabric Filter and ESPs

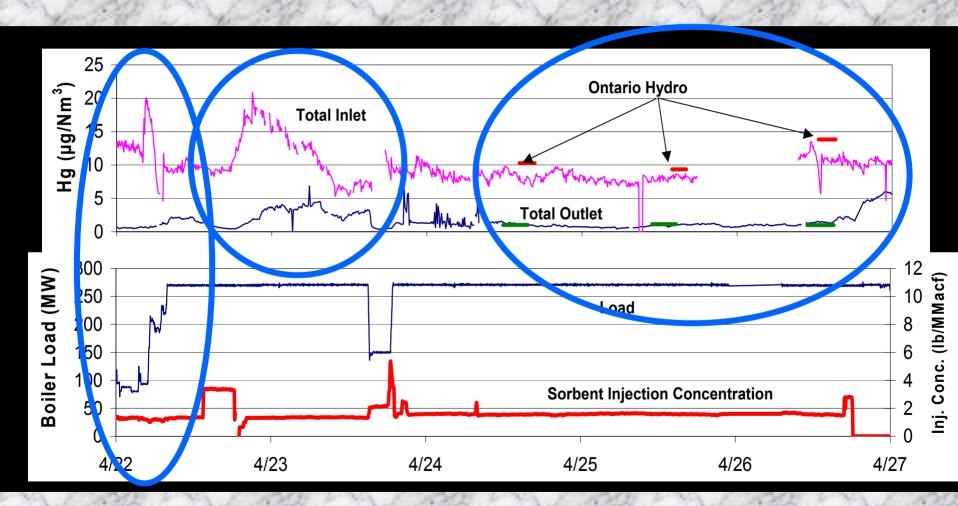




Issues with Variability of Inlet Hg Short-term vs. Long-term Results

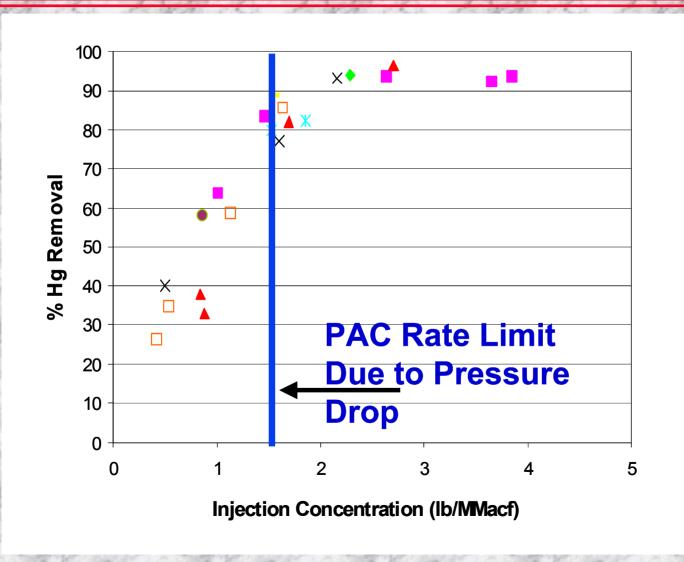


5-Day Continuous Injection





Mercury Removal vs. Injection Rate at Gaston





Conclusions: IPM Model Inputs for ACI on Bituminous and Subbituminous Coals

- 90 % Hg Removal
 - Bituminous coals: Fabric Filter (\$40/kW), ACI at 3 lb/Mmacf (0.4 mills/kWh)
 - ✓ Subbituminous coals: Fabric Filter, ACI at 3 lb/MMacf
 - ✓ Lignites: Flue Gas Cooling, Fabric Filter, ACI at 3 lb/MMacf
- 60 % HG Removal
 - ✓ Bituminous coals: ESP, ACI at 10 lb/Mmacf (1.2 mills/kWh)
 - ✓ Subbituminous coals: ESP, ACI at 10 lb/MMacf
 - ✓ Lignites: Flue Gas Cooling, ESP, ACI at 10 lb/MMacf
- Impact of Wet and Dry FGD on ACI
 - Bituminous coals: Reduces sorbent requirements
 - Subbituminous coals: Higher sorbent feedrate and/or more expensive sorbents
 - ✓ Lignites: Higher sorbent feedrate and/or more expensive sorbents



Future Plans

Long-term testing

_	Alabama Power	(Bituminous coal,	COHPAC FF)	2003-2004
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CCPI Program at WE Presque Isle (PRB, COHPAC FF) 2004-2006

Short-term testing at additional sites

_	* TBD Site (PRB with Spray Dryer)	9/2003
_	* TBD Site (PRB with small ESP)	3/2004
_	* TRD Site (Fastern Rituminous with Wet Scrubber)	9/2004

* Proposed

